



environment, forestry & fisheries

Department: Environment, Forestry
and Fisheries
REPUBLIC OF SOUTH AFRICA

Private Bag X 447, PRETORIA, 0001 · Environment House, 473 Steve Biko Street, Arcadia, 0083

Ref.: AEL/FS/ MKO-HGM/14/10/2019F

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ATMOSPHERIC EMISSION LICENCE AS CONTEMPLATED IN SECTION 43 OF THE NATIONAL ENVIRONMENTAL MANAGEMENT: AIR QUALITY ACT, (ACT NO. 39 OF 2004)

The Atmospheric Emission Licence issued to **Moab Khotsong Operations (Harmony Gold Mining Company)** in terms of section 42(1) of the National Environmental Management: Air Quality Act, 2004 (Act No. 39 of 2004) ("the Act"), in respect of Listed Activity No.4.1: **Drying and Calcining & 4.17: Precious and Base Metal Production and Refining**. The licence has been issued on the basis of information provided by the applicant, including amongst others, the licence application and the emission monitoring reports.

The licence is valid for a period of (five) **5** years from the date of issue.

The holder of the licence must, at least 60 days before the expiry date of the licence apply for the renewal of the licence by lodging an application in the form required by the licensing authority.

This current licence is a full licence for the facility.

The licence is issued subject to the conditions and requirements set out below which form part of the licence and are binding on the holder of the licence.

1. ATMOSPHERIC EMISSION LICENCE ADMINISTRATION

| | |
|--|--|
| Name of the Licensing Authority | National Department of Environment, Forestry and Fisheries |
| Atmospheric Emission Licence Number | AEL/FS/ MKO-HGM/14/10/2019F |
| Atmospheric Emission Licence Issue Date | 29 January 2021 |
| Atmospheric Emission Licence Type | Atmospheric Emission Licence |
| Atmospheric Emission Licence Expiry Date | 30 January 2026 |
| Review Date | Annually |

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2. ATMOSPHERIC EMISSION LICENCE HOLDER DETAILS

| | |
|--|--|
| Enterprise Name | Moab Khotsong Operations (Harmony Gold Mining Company) |
| Trading as | Moab Khotsong Operations |
| Enterprise Registration Number (Registration Numbers if Joint Venture) | 2006/039120/07 |
| Registered Address | Moab Khotsong Operations Harmony Gold Mining Company Limited Randfontein Office Park Cnr Main Reef Road and Ward Avenue, Randfontein, 1759 |
| Postal Address | Moab Khotsong Operations Harmony Gold Mining Company Limited P O Box 2, Randfontein, 1760 |
| Telephone Number (General) | (018)4784009 |
| Industry Sector | 07291 (Description: Mining of gold) |
| Name of Responsible Officer | Carlo Geel |
| Name of Emission Control Officer | Carlo Geel |
| Telephone Number | (018)4784009 |
| Cell Phone Number | 0835966741 |
| Fax Number | +27 11 692 3879 |
| Email Address | CGeel@Harmony.co.za |
| After Hours Contact Details | +27 83 5966741/ +27 73 3794221 |
| Land Use Zoning as per Town Planning Scheme | Mining |

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3. LOCATION AND EXTENT OF PLANT

| | |
|---|--|
| Physical Address of the Premises | Situated on Various portions of the farms; Zuiping 394, Crystalkop 69, Doornkom West 446, Mispah 274, Mispah 279, Moab 279 |
| Description of Site (Erf) | Harmony Gold Mining Company - Moab Khotsong Operations are located within the Fezile Dabi District Municipality, approximately 12km north and 10km south-east of Vierfontein and Klerksdorp, respectively, in the Free State Province. The land use in the area comprises primarily of mining and agriculture. Harmony Moab Operations are the main mining operation in the area. No environmentally sensitive areas have been identified. Administration buildings, workshops and site roads also form part of Harmony Gold – Moab Khotsong. |
| Coordinates of Approximate Centre of Operations | 26° 58.640' S 26° 46.000' E |
| Extent (km ²) | 9000 |
| Elevation Above Mean Sea Level (m) | 1315 |
| Province | Free State |
| Metropolitan/District Municipality | Fezile Dabi District Municipality |
| Local Municipality | Moqhaka Local Municipality |
| Designated Priority Area | NA |

3.1 Description of surrounding land use (within 5 km radius)

Harmony Gold Mining Company - Moab Khotsong Operations are located within the Fezile Dabi District Municipality, approximately 12km north and 10km south-east of Vierfontein and Klerksdorp, respectively, in the Free State Province. The land use in the area comprises primarily of mining and agriculture. Harmony Moab Operations are the main mining operation in the area. No environmentally sensitive areas have been identified.

The operations comprise of gold and uranium plants, a tailings storage complex, a waste rock dump, and two mine shafts as follows:

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- Noligwa and Mispah Gold Plant
- South Uranium Plant
- Great Noligwa Shaft
- Moab Shaft + Waste Rock Dump
- Mispah and Kopanang Pay Dam Tailings Storage Facilities

Administration buildings, workshops and site roads also form part of Harmony Gold – Moab Khotsong. Figure 1 below shows location of Harmony Gold Mining Company - Moab Khotsong Operations in relation to surrounding land use within 5km radius.

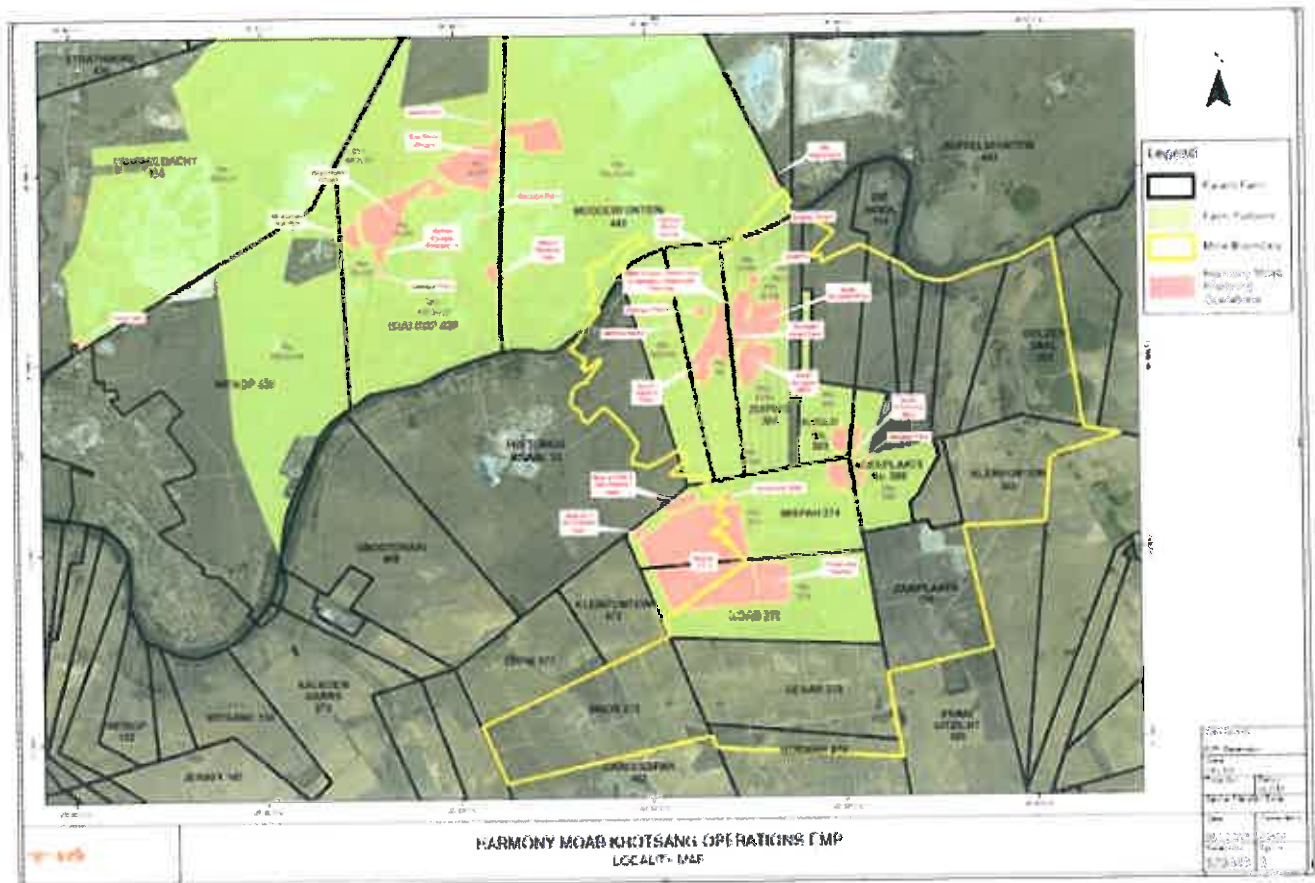


Figure 1: Location of Harmony Gold Mining Company - Moab Khotsong Operations in relation to surrounding land use within 5km radius

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4. GENERAL CONDITIONS

4.1 Process and ownership changes

The holder of the licence must ensure that all unit processes and apparatus used for the purpose of undertaking the listed activity in question, and all appliances and mitigation measures for preventing or reducing atmospheric emissions, are at all times properly maintained and operated.

- 4.1.1 No building, plant or site of works related to the listed activity or activities used by the licence holder shall be extended, altered or added to the listed activity without an environmental authorisation from the competent authority, where applicable. The investigation, assessment and communication of potential impact of such an activity must at least follow the basic assessment procedure as prescribed in the Environmental Impact Assessment Regulations published in terms of section 24(5) of the National Environmental Management Act, 1998 (Act No. 107 of 1998) (NEMA), as amended.
- 4.1.2 Any changes in processes or production increases, by the licence holder, will require prior approval by the licensing authority.
- 4.1.3 Any changes to the type and quantities of input materials and products, or to production equipment and treatment facilities will require prior written approval by the licensing authority.
- 4.1.4 The licence holder must, in writing, inform the licensing authority of any change of ownership of the enterprise. The licensing authority must be informed within 30 (thirty) days after the change of ownership.
- 4.1.5 The licence holder must immediately on cessation or decommissioning of the listed activity inform, in writing, the licensing authority.

4.2 General duty of care

- 4.2.1 The holder of the licence must, when undertaking the listed activity, adhere to the duty of care obligations as set out in section 28 of the NEMA.
- 4.2.2 The licence holder must undertake the necessary measures to minimize or contain the atmospheric emissions. The measures are set out in section 28(3) of the NEMA.
- 4.2.3 Failure to comply with the above condition is a breach of the duty of care, and the licence holder will be subject to the sanctions set out in section 28 of the NEMA.

4.3 Sampling and/or analysis requirements

- 4.3.1 Measurement, calculation and/or sampling and analysis shall be carried out in accordance with any nationally or internationally acceptable standard. A different method may be acceptable to the licensing authority as long as it has been consulted and agreed to the satisfactory documentation necessary in confirming the equivalent test reliability, quality and equivalence of analyses.

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4.3.2 The licence holder is responsible for quality assurance of methods and performance. Where the holder of the licence uses external laboratories for sampling or analysis, accredited laboratories shall be used.

4.4 General requirements for licence holder

4.4.1 The licence holder is responsible for ensuring compliance with the conditions of this licence by any person acting on his, her or its behalf, including but not limited to, an employee, agent, sub-contractor or person rendering a service to the holder of the licence.

4.4.2 The licence does not relieve the licence holder to comply with any other statutory requirements that may be applicable to the carrying on of the listed activity.

4.4.3 A copy of the licence must be kept at the premises where the listed activity is undertaken. The licence must be made available to the environmental management inspector representing the licensing authority who requests to see it.

4.4.4 The licence holder must inform, in writing, the licensing authority of any change to its details including the name of the emission control officer, postal address and/or telephonic details.

4.5 Statutory obligations

4.5.1 The licence holder must comply with the obligations as set out in Chapter 5 of the Act.

5. NATURE OF PROCESS: PROCESS DESCRIPTION

5.1 Nologwa Gold Plant

5.1.1 Ore Reception

Reef and Waste are hoisted at Moab Khotsong Mine using two 23.5ton ore skips. The reef is tipped into two silos with a capacity of 4500 tons each. The reef is drawn from the ROM Silos via Brute Force Vibrators onto the ROM mill feed conveyors. Great Nologwa Mine hoists around 200 000 ton reef a month. Reef can also be received from Moab Khotsong shaft via a rail transport system. There are normally seven 55ton hoppers per locomotive that tip into the Rail Bin with a capacity of 500ton. C1 conveyor then transfers the rock to the ROM Silos. Rock dump waste is also delivered to Nologwa Gold Plant via the rail transport system. The ore received from underground varies in size from rocks of 500mm to particles smaller than 1mm.

5.1.2 Milling

Two conveyors withdraw ore from the base of the ROM Silos and feed the two 6.71m diameter 10.06m long, trunnion supported ROM mills. The mills operate in closed circuit with a two-stage cyclone circuit. The solids are diluted to an RD of 1.1kg/l during the milling process. The main water source is the return water from the thickener section that circulates between the mills and thickeners. The milled product is extremely fine with 80% passing 75µm and less than 3% larger

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than 150m. The milled product is pumped to the thickener section where it passes over two linear screens (to remove wood-chips) before gravitating to the thickeners.

5.1.3 Thickeners

The milling product, with 85% to 90% moisture content, is pumped to the two Woodchip linear screens to remove woodchips. The underflow of the screens gravitates to the thickeners where solid-liquid separation takes place. Once separated, the water is returned to the Milling Plant to be used in the grinding process, and the thickened slurry is pumped to the Uranium Plant for uranium extraction.

The Thickener Plant has six 45m diameter thickeners. A slow-moving rake mechanism moves the settled slurry to the centre of the conical base from where it is pumped to the Uranium Plant. Around the top of the thickener, an overflow launder collects and removes the overflow water. Flocculants are added to the slurry to aid in the settling of the solid particles.

5.1.4 Neutralizing

Once the Uranium has been extracted from the pulp, it is returned to the Gold Plant. This pulp has an acidic pH of 1.5 to 2.5. If cyanide is added to slurry with a pH below 9.3, HCN gas formation will occur. This gas is known to be extremely toxic, thus resulting in a serious health and safety issue. To overcome this pH problem, slaked lime ($\text{Ca}(\text{OH})_2$) is added. The pH is increased in three stages from 1.5 to 7.5 in the first tank, 7.5 to 9.5 in the second tank and 9.5 to 10.5 in the third tank. Auto pH control is used to control the amount of lime added to effect neutralization. The liquid Sodium Cyanide is added to the pulp in the overflow launder of the fourth neutralizing pachuca. Oxygen is injected at No.2 neutralizing tanks via a circulation system. This is done to oxidize cyanide (mainly Ferrous) to reduce cyanide consumption. From here the slurry overflows into a tank from where it is pumped to the Safety Screening Plant.

5.1.5 Safety Screening

The Safety Screening Plant is an intermediate screening plant between the neutralizing and the leach section. Two 12m² Delkor Linear Screens and one Vibrator Screen are used to remove any woodchips and fibre that was not removed by the woodchip screens in the thickener section. The efficiency of the Kambalda Screens in the CIP and the Elution Column Strainers are severely hampered any woodchips and fibre.

5.1.6 Leaching

From the safety screens, the slurry is pumped to six flat bottomed mechanically agitated leach tanks. The cyanide concentration in the first tank is controlled by an on-line Cyanide analyser (TAC 2000) by controlling the cyanide addition in the neutralizing section. Liquid oxygen is injected via a circulation system into the first flat bottomed tank to increase the rate of leaching over the initial leaching stage. Oxygen is also injected at No.3 and No.5 flat-bottomed leach tanks via lances. From here the slurry is pumped to 16 air-agitated pachuca tanks to extend the leach

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process. The overall leach residence time is approximately 30 hrs. The leach tail is pumped to the CIP circuit.

5.1.7 Adsorption (CIP)

The Carbon In Pulp (CIP) section consists of 8 flat-bottomed adsorption vessels containing Activated Carbon Granules onto which the dissolved gold adsorbs. The slurry gravitates down the circuit from No.1 to No.8 tank. The carbon is pumped counter-current from No.8 to No.1 tank to increase the gold adsorbed from the pulp. The carbon from No.1 CIP tank is pumped onto a vibrator screen to screen out the slurry before the elution process. Regenerated carbon is pumped from the elution circuit back to No.8 CIP tank. To prevent the carbon from moving downstream with the slurry, Kambalda screens are installed in the tanks. The CIP residue gravitates from the last CIP tank on to two 12m² linear screens to recover fine carbon from the circuit. The overflow of the screens drops onto a vibrator screen where the overflow is bagged and the underflow is pumped to a drying tank. The underflow of the linear screens (residue slurry) is pumped to the backfill plant to produce backfill.

5.1.8 Elution and Carbon Circuit

The loaded carbon from No.1 CIP tank is dropped into two elution columns. A hot caustic solution (called eluant) is passed through the column to strip the gold from the carbon. This pregnant solution is now known as eluate and passes through electrowinning cells where the gold is electroplated onto stainless steel cathodes. A Zadra Elution Process is used where the caustic solution passes continuously through the column and the electrowinning cells. The barren eluant from the electrowinning cells is pumped back to the eluant tank from where it is re-circulated through the elution column. This process continues for the entire duration of the elution sequence, which is normally around 18 hours.

5.1.9 Recovery Section

The electrowinning section contains twelve Mintek type cells. Each cell has six cathodes and seven anodes. The cathodes consist of stainless-steel wire mesh packed in a stainless-steel frame. The anodes consist of a framework of stainless-steel flat bars. Six rectifiers are used to control the current at 600 Amps and the voltage at 12 Volts. The eluate from the elution column passes through a flash tank and then a distribution manifold providing equal flow to each of the twelve cells. The dissolved gold in the eluate is electrowon onto the cathodes. The spent electrolyte then flows through to the eluant tank to be re-circulated to the elution column.

5.1.10 Backfill

The CIP residue is pumped from the CIP residue tank to two feed tanks in the backfill section that feeds the primary cluster cyclone feedboxes. Here the density of the slurry is kept at 1.2 kg/l and pumped through two cluster cyclones for upgrading purposes. The underflow of the cyclones is pumped to the feed to float tank and pumped to the neutralizing tanks. The overflow of these cyclones is fed to the three backfill thickeners, where the RD is increased to about 1.5 kg/l. Flocculants are added here. The underflow of the backfill thickeners is pumped to the two reject

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tanks, and the thickener overflow is pumped to the water thickener. The overflow of the water thickener is used as process water.

5.2 Mispah Plant

5.2.1 Ore Reception

The ore reception section receives ore from rail, truck and conveys it to the 3B bin. The level of ore in the bin is measured by a laser level measurement device. This is provided to allow control to be implemented to prevent the bin being pulled completely empty.

From the bin, ore is fed by a vibrating feeder onto CV01 conveyor to three 3B bins. The weight of ore conveyed from the bin is measured by a weight meter. Dust extraction is provided to remove dust generated as ore is tipped from the feeder onto the conveyor. To ensure adequate ventilation air is blown into the tunnel under the rail bin by a forced ventilation fan. Provision is also made for spraying water at the tipping point into the rail bin, at the tipping point from the feeder onto the belt and at the discharge from the head of the belt. Dust suppression sprays that can be manually opened are utilized when dry dusty ore is being handled.

5.2.2 Milling

Ore is fed from 3B bin conveyor onto the mill feed conveyor and into the mill. Milled product exits via the grates at the end of the mill. Oversize material in the mill discharge is removed by the trommel screen and routed to the recycle conveyor system. Trommel screen undersize flows into the mill discharge where it is diluted by mill return water and pumped to the primary cyclones. The primary cyclone underflow is recycled to the mill for further comminution. Primary cyclone overflow gravitates to the secondary cyclone for further classification. Secondary cyclone underflow is routed to the mill discharge sump and overflow to the O/F pump box from where it is pumped to the woodchip screening section.

5.2.3 Woodchip screening and thickeners

Cyclone overflow is pumped to the woodchip screen and lime is added prior to screening to allow coarse material in the lime to be screened. Screened slurry gravitates to the thickeners, while oversized materials are washed by sprays on the screen. The oversize materials drop onto a vibrating screen; coarse material screened out on the high-grade woodchip screens is also pumped to the same vibrating screen, where it is dewatered. De-watered oversize material drop onto a conveyor to be deposited on a stockpile. Water is pumped to the high-grade woodchip screens distribution box. Scale forming in the apertures of the woodchip screen is periodically removed by spraying with high pressure water.

5.2.4 Leaching

Thickened slurry is pumped to the first leach tank at a controlled RD. RD control is achieved by adding dilution water to the leach feed pump box to achieve a set RD as measured by a densitometer on the leach feed line. Prior to flowing into the first tank, the slurry is sampled by

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passing through a primary crosscut sampler. The sample is further sub-divided by a secondary vezin sampler. In the first tank, the pH is raised to >10.5 by addition of lime from a ring main. Cyanide is added to the second tank; cyanide addition rate is controlled to achieve a set cyanide concentration. Addition rate is determined both by measurement of the actual concentration and the mass flow into the circuit.

5.2.5 Carbon in Pulp

Slurry is received from the leach via the CIP feed pump. The slurry exposed to cyanidation meets activated carbon and the dissolved mineral absorbs onto the carbon. The slurry cascades down the CIP tanks. Carbon enters the CIP circuit at the last CIP tank on-line from the elution building via the acid washed carbon transfer pump. The carbon migrates upstream with the use of carbon transfer pumps. The interstage MPSP screens prevent the coarse carbon particles to short circuit with the slurry stream. Loaded carbon is returned from the first CIP tank with the carbon transfer pump to the loaded carbon screen. The carbon concentration as measured by the carbon analysers in each CIP tank is controlled by the carbon transfer pump. Each CIP tank has an on-line/off-line selection switch that enables the operator to take a tank offline without impacting on the normal operation of the circuit.

5.2.6 Elution and Regeneration

Eluted carbon from the elution column is sent to the regeneration kiln feed bin where process water is added. The underflow is discharged to the screw feeder for dewatering and fed to the regeneration kiln. The quench tank receives the overflow from the regeneration kiln feed bin and hot carbon from the regeneration kiln. Regenerated carbon is quenched in the quench tank, and then pumped to the existing carbon acid wash screen. The overflow in the quench tank is recycled to the process.

5.3 **South Uranium Plant**

The Uranium Plant was commissioned in 1979 and was originally designed to process 240 000 tons per month.

5.3.1 Leach Section

Thickened pulp is received from Nologwa Gold Plant at a density 1.550 kg/l. The increased RD benefits reagent consumption (manganese dioxide as oxidizing agent and sulphuric acid as lixiviant). Each pachuca holds 762m³ volume of material. The pulp is fed directly to either No. 1 or No. 2 Pachuca (depending on which is first in line). Recycled acid ($\pm 60\text{g/l H}_2\text{SO}_4$), from the Solvent extraction section, is added to the first pachuca. Sulphuric acid (98% pure) is added into the second (90%) and third (10%) pachucas. The sulphuric acid neutralizes carbonate minerals found in the ore and is used as lixiviant in the dissolution of uranium.

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5.3.2 Counter Current Decantation (CCD)

The purpose of the CCD circuit is to separate gold bearing slurry from uranium bearing solution, whilst in the process washing most of the available dissolved uranium from the slurry phase into the clear solution phase. This process occurs in the CCD circuit consisting of six thickeners (five of which are operating as per norm and one being operated as a clarifier.) CCD1's diameter is 60m and CCD 2- 6's diameters are 55m. CCD2-6 holds approximately 300m³ of slurry and 11 000m³ of solution. CCD 1 holds approximately 12 000m³ of solution as it is only used as a clarifier.

5.3.3 Counter Current Ion Exchange (CCIX)

The purpose of the CCIX section is to reduce the volume of uranium bearing solution to be treated in the Solvent Extraction (SX) section in the plant. This is done by concentrating uranium in the eluate. For this purpose, resin is used as transfer medium for the uranium from the high volume pregnant solution to the lower volume eluate. The CCIX section at the South Uranium Plant consists of five independently operated resin treatment streams. Pregnant solution from the CCD circuit gravitates to the CCIX circuit where it is deposited into two pregnant solution tanks. The pregnant solution is then pumped upwards (at a flow rate of 160 m³/hr per column) through the five adsorption columns.

5.3.4 Solvent Extraction Section

The purpose of the solvent extraction section is to further purify and concentrate the uranium in the OK liquor suitable for treatment in the ADU section. The eluate from the CCIX section is pumped to the SX section at a flow rate of 18m³/hr.

5.3.5 Ammonium Di-Uranate Precipitation (ADU)

The OK liquor from the extractors in the SX section is pumped to the precipitator tank. In this tank, ammonia gas in combination with compressed air is added to allow the precipitation of the Ammonia Di-Uranate [(NH₄)₂U₂O₇]. The tank is mechanically agitated to ensure that no settlement occurs inside the tank. The pH of the slurry from the precipitation tank needs to remain at pH 7.2 as this is beneficial to the precipitation of the ADU.

All sources of potential atmospheric emissions, including the process description at Harmony Gold-Moab Khotsong Operations have been identified and a summary thereof provided in Figures 2 and 3 below:

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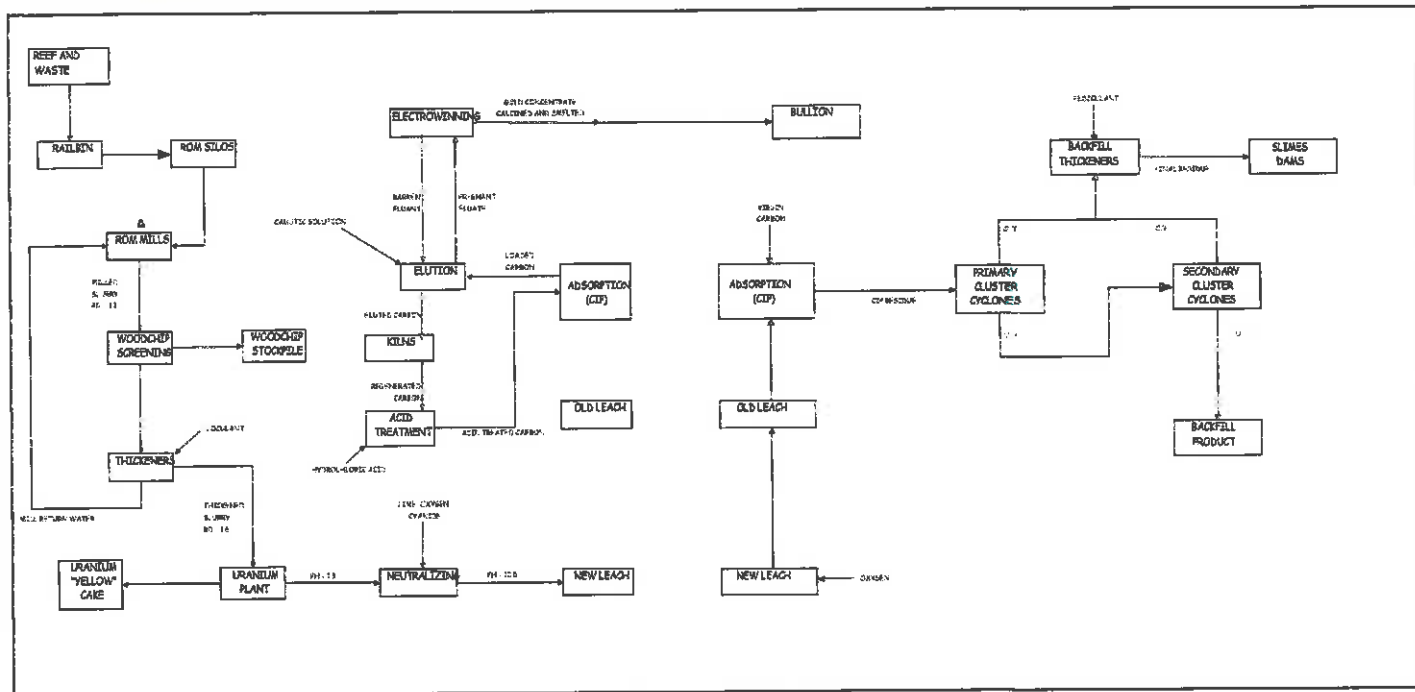


Figure 2: Mispah and Norigwa Gold Plants Process Flow Diagram

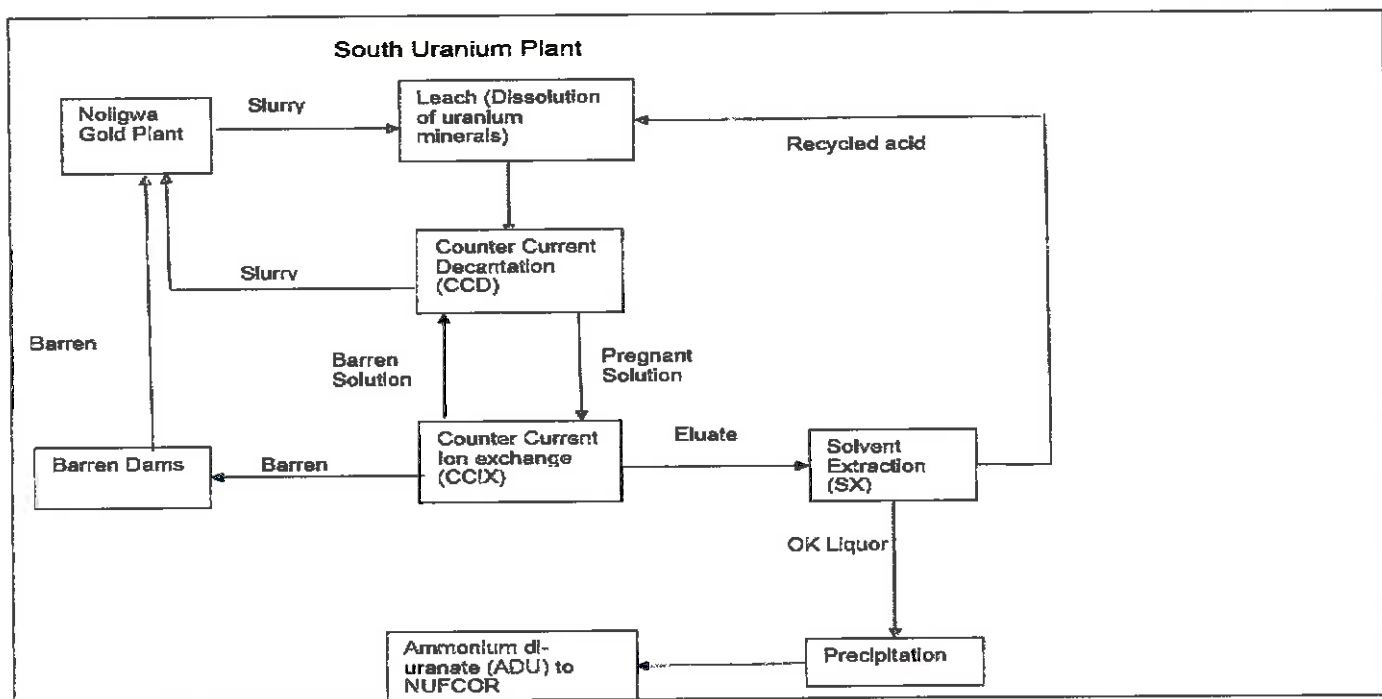


Figure 3: South Uranium Plant Process Flow Diagram

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5.4 Listed activity or activities

List of all Listed Activities, as published in terms of Section 21 of the AQA, authorised to be conducted at the premises by the licence holder:

| Listed Activity Number | Category of Listed Activity | Sub-category of the Listed Activity | Listed Activity Name | Description of the Listed Activity |
|------------------------|-----------------------------|-------------------------------------|---|--|
| 1 | 4 | 4.1 | Drying and Calcining | Drying and calcining of mineral solids including ore. |
| 2 | 4 | 4.17 | Precious and Base Metal Production and Refining | The production or processing of precious and associated base metals through chemical treatment (Excluding Inorganic Chemicals-related activities regulated under Category 7) |

5.5 Unit process or processes

List of all unit processes associated with the listed activities to be undertaken at the site of work.

| Unit Process | Unit Process Function | Batch or Continuous Process |
|---------------------------|--|-----------------------------|
| Noligwa Gold Plant | | |
| Ore Reception | Reef is received from underground via ore skips and also from Moab Khotsong shaft via rail transport system. | Continuous |
| Milling | Ore solids are diluted to an RD of 1.1kg/l to extremely fine solids of which 80% is 75 µm and less than 3% is larger than 150 µm | Continuous |
| Screening | Milled product (which has 80-90% moisture content) is pumped to woodchip linear screens to remove wood chips. | Continuous |
| Thickening | Pre-screened ore product gravitates to the thickener where liquid is separated from the solid. Once separated, water is returned to the milling plant for the milling process. | Continuous |
| Neutralising | Involves the addition of slake lime (Ca (OH) ₂) to an acidic gold pulp in order increase its pH up to 10.5 before the addition of cyanide. This is done to avoid | Continuous |

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| Unit Process | Unit Process Function | Batch or Continuous Process |
|-----------------------------|--|-----------------------------|
| | the formation of HCN gas. | |
| Safety Screening | Removal of wood chips and fibre from the neutralised gold pulp | Continuous |
| Leaching | Addition of cyanide and liquid oxygen into the neutralised gold pulp | Continuous |
| Adsorption (Carbon in Pulp) | Dissolved gold is adsorbed by the 8 flat-bottomed adsorption vessels which consist of activated carbon granules. | Continuous |
| Elution and Carbon Circuit | The loaded carbon is sent to the elution columns, where the stripping of gold from carbon takes place. An electric current is applied to the pregnant solution (from elution process) to precipitate gold onto cathodes. Caustic solution is added to increase the conductivity of the solution. | Batch |
| Carbon Regeneration | Eluted carbon is then sent to the kilns to be regenerated so that it can be used again in the adsorption process. The moisture and impurities are removed, and the carbon pores are opened. | Continuous |
| Recovery/Electrowinning | The eluate from the elution circuit is passed through a flash tank and then a distribution manifold providing equal flow to each of the eighteen cells. The dissolved gold in the eluate is electrowon onto the stainless steel in the cathode baskets. The spent electrolyte then flows through to the eluent tank to be re-circulated to the elution column. | Batch |
| Calcining | Gold bearing sludge from the electrowinning process is sent to the calcining ovens for drying and removal of impurities from the concentrated product before smelting. | Batch |
| Gold Smelting | Smelting of gold concentrate in crucible furnaces. Additives are added to the smelting furnace to remove impurities, forming a slag. Molten gold is then cast into moulds to form gold dore (bars) | Batch |
| Backfill | The CIP residue is pumped to two feed tanks which feed the primary cluster | Batch |

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| Unit Process | Unit Process Function | Batch or Continuous Process |
|-----------------------------|---|-----------------------------|
| | cyclone feed-boxes. The density of the slurry is kept at 1.2 kg/l and pumped through two cluster cyclones for upgrading purposes. The underflow of the cyclones is pumped to the feed float tank and this product goes to the flotation plant. The overflow of these cyclones is fed to the three backfill thickeners, where the RD is increased to about 1.5 kg/l. | |
| Mispah Plant | | |
| Ore Reception | Ore is received from rail, truck or grasshopper conveyers to 3B bin and measured. Dust extraction removes dust generated during tipping of ore from the feeder. | Continuous |
| Milling | Ore is processed to fine product which exits via grates at the end of the mill. Oversized material is removed by a trommel screen and routed to the recycle conveyer system. | Continuous |
| Screening and thickening | Milled product is pumped to the woodchip screen to remove wood chips, grit, plastic, etc. Oversized material is washed and screened out on the high-grade woodchip vibrating screens where it is de-watered. | Continuous |
| Leaching | Addition of cyanide and liquid oxygen into the neutralised gold pulp. | Continuous |
| Adsorption (Carbon in Pulp) | Dissolved gold is adsorbed by 8 flat-bottomed adsorption vessels, which consist of activated carbon granules. | Continuous |
| Elution | The loaded carbon is sent to the elution columns, where the stripping of gold from carbon takes place. An electric current is applied to the pregnant solution (from elution process) to precipitate gold onto cathodes. Caustic solution is added to increase the conductivity of the solution. | Batch |
| Carbon regeneration | Eluted carbon from elution column is sent to the kiln where water is added. The underflow is discharged to the screw feeder for dewatering and fed to the regeneration | Continuous |

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| Unit Process | Unit Process Function | Batch or Continuous Process |
|--------------------------------------|---|-----------------------------|
| | kiln. The regenerated carbon is washed in the carbon acid wash and recycled to be used again in the adsorption process. | |
| South Uranium Plant | | |
| Leaching | Uranium in the pulp is dissolved through the addition of manganese dioxide and sulphuric acid. Pulp is agitated to keep it suspended and to ensure sufficient mixing of reagents and pulp in order to facilitate dissolution of uranium. | Continuous |
| Counter Current Decantation | Application of thickeners to extract uranium (before gold extraction) in order to reduce uranium- and gold loss. | Continuous |
| Counter current ion exchange process | The production of a uranium bearing solution through adsorption of uranium onto resin and stripping it again from the resin. | Continuous |
| Solvent extraction | The eluate is purified and converted into a suitable form for treatment in the ammonia precipitation plant. Uranium is transferred to a solvent phase in the extractors and washed with water in the scrub. Uranyl sulphate is then stripped from solvent and transferred to an aqueous phase known as OK liquor. | Continuous |
| Uranium Precipitation | The OK liquor containing uranyl sulphate is precipitated with ammonia gas to form a uranium precipitate in the form of ammonium di-uranate. The precipitate is washed of impurities and transferred to NUF COR for processing and exportation. | Continuous |

5.6 Hours of operations

Hours of operation of all unit processes associated with the listed activities at the site of work.

| Unit Process | Operating Hours | Days of Operation per Year |
|----------------------|-----------------|----------------------------|
| Noligwa Plant | | |
| Ore Reception | 00h00-24h00 | 365 |
| Milling | 00h00-24h00 | 365 |
| Screening | 00h00-24h00 | 365 |

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| Unit Process | Operating Hours | Days of Operation per Year |
|--------------------------------------|-----------------|----------------------------|
| Thickening | 00h00-24h00 | 365 |
| Neutralising | 00h00-24h00 | 365 |
| Safety Screening | 00h00-24h00 | 365 |
| Leaching | 00h00-24h00 | 365 |
| Adsorption (Carbon in Pulp) | 00h00-24h00 | 365 |
| Elution and Carbon Circuit | 00h00-24h00 | 365 |
| Carbon Regeneration | 00h00-24h00 | 365 |
| Recovery | 00h00-24h00 | 365 |
| Calcining | 00h00-24h00 | 365 |
| Gold Smelting | 07h00-10h00 | 100 |
| Backfill | 00h00-24h00 | 365 |
| Mispah Plant | | |
| Ore Reception | 00h00-24h00 | 365 |
| Milling | 00h00-24h00 | 365 |
| Screening and thickening | 00h00-24h00 | 365 |
| Leaching | 00h00-24h00 | 365 |
| Adsorption (Carbon in Pulp) | 00h00-24h00 | 365 |
| Elution | 00h00-24h00 | 365 |
| Carbon Regeneration | 00h00-24h00 | 365 |
| South Uranium Plant | | |
| Leaching | 00h00-24h00 | 365 |
| Counter Current Decantation | 00h00-24h00 | 365 |
| Counter current ion exchange process | 00h00-24h00 | 365 |
| Solvent extraction | 00h00-24h00 | 365 |
| Uranium Precipitation | 00h00-24h00 | 365 |

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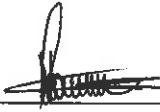
6 RAW MATERIALS AND PRODUCTS

6.1 Raw materials used

| Raw Material Type | Maximum Permitted Consumption Rate (Quantity) | Design Consumption Rate (Quantity) | Actual Consumption Rate (Quantity) | Units (Quantity/Period) |
|----------------------------|---|------------------------------------|------------------------------------|-------------------------|
| Noligwa Gold Plant | | | | |
| Ore | 260 000 | 260 000 | 120 000 | tons/month |
| Reagents (caustic) | 90 | 90 | 60 | tons/month |
| Reagents (cyanide) | 90 | 90 | 51 | tons/month |
| Hydrochloric Acid | 75 | 75 | 60 | tons/month |
| Residue | 260 000 | 260 000 | 120 000 | tons/month |
| Mispah Gold Plant | | | | |
| Ore | 147 000 | 147 000 | 130 200 | tons/month |
| Reagents (caustic) | 40 | 40 | 25 | tons/month |
| Reagents (cyanide) | 40 | 40 | 30 | tons/month |
| Hydrochloric Acid | 18 | 18 | 10 | tons/month |
| Residue | 147 000 | 147 000 | 130 200 | tons/month |
| South Uranium Plant | | | | |
| Coal | 1 650 | 1 650 | 0 | tons/month |
| Sulphuric Acid | 8 000 | 8 000 | 2 600 | tons/month |
| Manganese | 1 300 | 1 300 | 624 | tons/month |

| Regulated Raw Materials* | | |
|---------------------------------|---|-------------------------|
| Raw Material Type | Maximum Permitted Consumption Rate (Quantity) | Units (quantity/period) |
| Recovered Tailings | 1500 | Tons per hour |
| Ore | 407 000 | Tons per month |

* Regulated raw materials refers to those materials when increased or decreased may result in the change of air emissions output.

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6.2 Production rates

| Production Name | Maximum Production Capacity Permitted (Quantity) | Design Production Capacity (Quantity) | Actual Production Capacity (Quantity) | Units (Quantity/Period) |
|------------------------|--|---------------------------------------|---------------------------------------|-------------------------|
| Gold Bullion (Noligwa) | 1200 | 1200 | 750 | kg/month |
| Gold bullion (Mispah) | 100 | 100 | 35 | kg/month |
| By-Product Name | Maximum Production Capacity Permitted (Quantity) | Design Production Capacity (Quantity) | Actual Production Capacity (Quantity) | Units (Quantity/Period) |
| ADU (yellow cake) | 70 | 70 | 22 | tons/month |

6.3 Materials used in energy sources

| Materials for Energy | Sulphur Content of the Material (%) | Ash Content of Material (%) | Maximum Permitted Consumption Rate (Quantity) | Design Consumption Rate (Quantity) | Actual Consumption Rate (Quantity) | Units (Quantity/Period) |
|-----------------------------------|-------------------------------------|-----------------------------|---|------------------------------------|------------------------------------|-------------------------|
| Electricity (Noligwa and Mispah) | 0 | 0 | 2 550 | 2 550 | 1 275 | kWh |
| Electricity (South Uranium Plant) | 0 | 0 | 2 000 000 | 2 000 000 | 1 528371.33 | kWh/month |

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6.4 Sources of atmospheric emission

6.4.1 Point source parameters

| Point Source Code | Source Name | Latitude (decimal degrees) | | Longitude (decimal degrees) East | Height of Release Above Ground (m) | Height Above Nearby Building (m) | Diameter at Stack Tip / Vent Exit (m) | Actual Gas Exit Temperature (°C) | Actual Gas Volumetric Flow (m ³ /hr) | Actual Gas Exit Velocity (m/s) | Emission Hours | Type of Emission (Continuous / Batch) |
|-------------------|---|----------------------------|--------------|----------------------------------|------------------------------------|----------------------------------|---------------------------------------|----------------------------------|---|--------------------------------|------------------|---------------------------------------|
| | | South | East | | | | | | | | | |
| EU0001 | Noligwa Gold Plant Carbon Regeneration Kiln 1 Stack | 26°57'45.14" | 26°46'50.46" | 26°46'50.46" | 25 | 1 | 0.2 | 40.4 | 192 | 1.7 | 24 hours per day | Continuous |
| EU0002 | Noligwa Gold Plant Carbon Regeneration Kiln 2 Stack | 26°57'45.03" | 26°46'49.96" | 26°46'49.96" | 25 | 1 | 0.2 | 31.4 | 270 | 2.4 | 24 hours per day | Continuous |
| EU0003 | Noligwa Gold Plant Carbon Regeneration Kiln 3 Stack | 26°57'44.93" | 26°46'49.15" | 26°46'49.15" | 25 | 1 | 0.2 | 290.7 | 258 | 2.3 | 24 hours per day | Continuous |
| EU0004 | Noligwa Gold Plant Smelting Furnaces Stack | 26°57'46.74" | 26°46'49.87" | 26°46'49.87" | 20 | 2 | 0.4 | 43.3 | 3 440 | 8.5 | 24 hours per day | Continuous |

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| Point Source Code | Source Name | Latitude (decimal degrees) | Longitude (decimal degrees) | Height of Release | Height Above Nearby | Diameter at Stack Tip / Vent | Actual Gas Exit Temperature | Actual Gas Volumetric Flow (m ³ /hr) | Actual Gas Exit Velocity | Emission Hours | Type of Emission (Continuous) |
|-------------------|--|----------------------------|-----------------------------|-------------------|---------------------|------------------------------|-----------------------------|---|--------------------------|------------------|-------------------------------|
| EU0005 | South Uranium Plant Boiler Stack (less than 50MW net heat input) | 26°58.4'55" | 26°46'27.97" | 20 | 15 | 2.14 | 156 | 81330 | 6.3 | 24 hours per day | Continuous |

Note: Stack parameters (temperature, flow rate, gas exit velocity) estimated based on existing plant details.

6.4.2 Area and/or line source parameters

| Area Source Code | Source Name | Source Description | Latitude (decimal degrees) of SW corner | Longitude (decimal degrees) of SW corner | Height of Release Above Ground (m) | Length of Area (m) | Width of Area (m) | Emission Hours | Type of Emission (Continuous / Intermittent) |
|------------------|---|---------------------------------------|---|--|------------------------------------|--------------------|-------------------|------------------|--|
| A001 | South Uranium Plant Coal stockpile area | Coal off-loading & loading operations | 26°58'01"S | 26°46'29.27"E | 3 | 1.40 | 1.40 | 24 hours per day | Intermittent |
| A002 | Mispah Tailings Storage Facility | Slurry deposition site | 26°59'49.51"S | 26°46'29.86"E | 9 | 1 386 | 992 | 24 hours per day | Intermittent |

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7 APPLIANCES AND MEASURES TO PREVENT AIR POLLUTION

7.1 Appliances and control measures

| Associated Source Code | Appliances | | Abatement Equipment Control Technology | | | | | | | | |
|------------------------|--|---------------|--|---------------------------|------------------|-----------------|--|-----------------|-----------------------------|--------------------------------|-------------------------|
| | Equipment Number | Serial Number | Appliance Type | Technology Name and Model | Manufacture Date | Commission Date | Date of Significant Modification / Upgrade | Technology Type | Design Capacity | Minimum Control Efficiency (%) | Minimum Utilization (%) |
| EU0004 | Patent number: CC89/1123 0/23; Fan equipment number: RFA01 | 1006298 | Bag filters | CD001 | 2009 | 11 March 2009 | NA | Baghouse | 100%(7.5 m ³ /s) | 98 | 95 |

7.1.1 95% minimum utilization allows 5% downtime for unplanned maintenance and repairs.

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7.2 Point source – maximum emission rates (under normal working conditions*)

| Point Source Code | Pollutant Name | Maximum Release Rate (mg/Nm ³) | Date to be Achieved By | | Duration of Emissions |
|-------------------|-----------------|--|------------------------|----------------|-----------------------|
| | | | | Average Period | |
| EU0001 | PM | 50 | Immediately | Hourly | 24 hrs/day |
| EU0002 | SO ₂ | 1000 | Immediately | Hourly | 24 hrs/day |
| EU0003 | NOx | 500 | Immediately | Hourly | 24 hrs/day |
| EU0004 | NH ₃ | 100 | Immediately | Hourly | 24 hrs/day |
| | Cl ₂ | 50 | Immediately | Hourly | 24 hrs/day |
| | HCl | 30 | Immediately | Hourly | 24 hrs/day |
| | HF | 30 | Immediately | Hourly | 24 hrs/day |
| | NOx | 300 | Immediately | Hourly | 24 hrs/day |
| EU0005** | PM | 50 | Immediately | Hourly | 24 hrs/day |
| | SO ₂ | 400 | Immediately | Hourly | 24 hrs/day |
| | SO ₂ | 2800 | Immediately | Hourly | 24 hrs/day |
| | PM | 120 | Immediately | Hourly | 24 hrs/day |

* Under normal conditions of 273K, 101.3 kPa, and 10% O₂.

** Small boiler unit (less than 50MW net heat input): To be managed in terms of S23 of the Air Quality Act.

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7.2.1 Point source – operating requirements

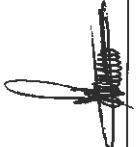
The emission testing to be conducted during under normal operating conditions

7.3 Point source – maximum emission rates (under start-up, maintenance and shut-down conditions)

| Point Source Code | Source Name | Description of Occurrence of Potential Releases | Timeframe for Implementation of Specific Measures | Pollutants and associated amount of emissions | Method of Monitoring/Measure of Effectiveness | Briefly Outline Back Up Plan |
|-------------------|---------------------|---|---|---|---|------------------------------|
| EU0001 | As described in 6.4 | Power failure | Immediately | PM, SO ₂ , NO _x , | Visual inspection, dark smoke | Shutdown |
| EU0002 | As described in 6.4 | Power failure | Immediately | PM, SO ₂ , NO _x , HCl, Cl ₂ , NH ₃ , HF | Visual inspection, dark smoke | Shutdown |
| EU0003 | As described in 6.4 | Power failure | Immediately | PM, SO ₂ | Visual inspection, dark smoke | Shutdown |

7.3.1 Point source – operating requirements

Should normal start-up, maintenance, upset and shut-down conditions exceed a period of 48 hours, Section 30 of the National Environmental Management Act (Act no.107 of 1998) shall apply.

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7.4 Point source – emission monitoring and reporting requirements

| Point Source Code | Emission Monitoring Method | Sampling Duration | Sampling Frequency | Parameters to be Measured | Parameters to be Reported | Reporting Frequency |
|----------------------------|----------------------------|-------------------------|--------------------|---|--|--|
| EU0001 EU0002 EU0003 | As per NEM: AQA Annexure A | 3X tests, each one hour | Biannually | PM, NOx, SO ₂ | PM, NOx, SO ₂ | Thirty (30) days after sampling/ monitoring |
| EU0004 | As per NEM: AQA Annexure A | 3X tests, each one hour | Biannually | PM, NOx, SO ₂ , NH ₃ , Cl ₂ , HCl, and HF | PM, NOx, SO ₂ , NH ₃ , Cl ₂ , HCl, and HF | Thirty (30) days after sampling/ monitoring |
| EU0005 | As per NEM: AQA Annexure A | 3X tests, each one hour | Biannually | PM, SO ₂ | PM, SO ₂ | Thirty (30) days after sampling/ monitoring |

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7.5 Area and/or line source – management and mitigation measures

| Area and/or Line Source Code | Area and/or Line Source Description | Description of Specific Measures | Timeframe for Achieving Required Control Efficiency | Method of Monitoring Measures Effectiveness | Contingency Measures |
|------------------------------|---|---|---|---|--|
| A001 | South Uranium Plant Coal stockpile area - Coal off - loading & loading operations | Regular inspection and wet suppression of stockpiles where necessary (including wind shielding, storage away from site boundaries, and restricted height of stockpiles) | Upon commencement of the listed activities | ASTM D1739: 1970 Method | No loading/offloading during high wind condition |
| A002 | Mispah Tailings Storage Facility - Slurry deposition site | A dust fall monitoring programme will be implemented | Upon commencement of the listed activities | ASTM D1739: 1970 Method* | No loading/offloading during high wind condition |

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8. ROUTINE REPORTING AND RECORD-KEEPING

8.1 Complaints register

- 8.1.1 The licence holder must maintain a complaints register at its premises, and such register must be made available for inspections. The complaints register must include the following information on the complainant, namely, the name; physical address; telephone number; date and the time when the complaint was registered. The register should also provide space for noise, dust and offensive odours complaints.
- 8.1.2 Furthermore, the licence holder is to investigate and, monthly, keep record in a summarised format on the total number of complaints logged. The complaints must be reported in the following format with each component indicated as may be necessary:
- Source code / name;
 - Root cause analysis;
 - Calculation of impacts / emissions associated with incidents and dispersion modelling of pollutants, where applicable;
 - Measures implemented or to be implemented to prevent recurrence; and
 - Date by which measure will be implemented.
- 8.1.3 The licensing authority must also be provided with a copy of the complaints register. The record of a complaint must be kept for at least 5 (five) years after the complaint was made.

8.2 Reporting

- 8.2.1 The licence holder must complete and submit to the licensing authority a biannual report. The report must include information for the period under review (i.e. six monthly after the date of issue of the licence). The report must be submitted to the licensing authority not later than 30 (thirty) days after the end of each reporting period. The report must include, amongst others, the following items:
- Pollutant emissions trend;
 - Dust fallout monitoring report prepared in terms of Section 5 of the National Dust Control Regulations (Regulations No. R 827 of 1 November 2013);
 - Compliance audit report(s), showing compliance with the licence conditions; and
 - Major upgrades projects (i.e. abatement equipment or process equipment), where applicable
- 8.2.2 The licence holder must report greenhouse gas emissions in terms of the National Greenhouse Gas Reporting Regulations, 2017 (Government Notice No 275 of 3 April 2017).

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9. DISPOSAL OF WASTE AND EFFLUENT ARISING FROM ABATEMENT EQUIPMENT CONTROL TECHNOLOGY

9.1 The disposal of any waste and effluent arising from the abatement equipment control technology must comply with the relevant legislation and requirements of the relevant authorities.

| Source Code / Name | Waste / Effluent Type | Hazardous Components Present | Method of Disposal |
|--|-----------------------|--------------------------------------|--|
| EU0004 (baghouse linked to smelting furnaces stack) | Dust from baghouse | Possible traces of cyanide and acids | Sold to Rand Refinery/ disposed at relevant waste disposal site |

10. PENALTIES FOR NON-COMPLIANCE WITH LICENCE AND STATUTORY CONDITIONS OR REQUIREMENTS

10.1 Failure to comply with any of the licence and relevant statutory conditions and/or requirements is an offence, and the licence holder, if convicted, will be subjected to those penalties as set out in section 52 of the AQA.

11. APPEAL OF LICENCE

11.1 The licence holder must notify registered interested and affected parties of the issuance of this licence, in writing and within fourteen (14) days, of receiving the Department's decision.

11.2 The notification referred to in 11.1 must –

- Specify the date on which the licence was issued;
- Inform the registered interested and affected parties of the appeal procedure provided for in the National Appeal Regulations, GN 993 of 08 December 2014; and
- Advise the interested and affected parties that a copy of the licence will be furnished on request.

11.3 An appeal against the decision may be lodged with the Minister in terms of the National Appeal Regulations GN 993 of 08 December 2014 within 20 days from the date of this license, and directed to: Director: Appeals and Legal Review, Department of Environmental Affairs, Private Bag X447, PRETORIA, 0001, Tel No.: 012 399 9626, Email address: AppealsDirectorate@environment.gov.za.

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